

ADDITIONAL FLUORINATION OF PARTLY FLUORINATED ORGANIC COMPOUNDS BY ELEMENTAL FLUORINE / AN OBTAINING METHOD FOR PRACTICAL PURPOSES FLUORINE MATERIALS

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(continuation)

2. Perfluorinated Organic Compounds Purification

Data listed above allowed us to draw an assumption, that such an approach can be successfully used for deep purification of perfluorinated compounds ("crude materials") obtained using ECF method. All known methods are based on destruction of hydrogen containing admixtures. It is necessary to take into account that their content in the reaction mixtures reaches 30%, then these methods are not recognized as wholly satisfactory. Another approach for purification of PFOC (perfluorinated organic compounds) is in additional fluorination of hydrogen containing admixtures. This approach implementation allows increasing of yield of PFOC, lowering of waste products, simplifying the process and as a result decreasing the cost of target products.

The known method of purification is in high concentration aqua alkali (85-90%) treatment at 100-120 °C. This method has a number of essential disadvantages, which hampers its application in production. Among them are: a need of working under pressure of 13-15 bar, high melting point of high concentration alkali and a related to that danger of blocking armature and communications, and also a need to use special alloys for reactor making, as common stainless steel are up to corrosive cracking [58] and [59], that water displacement by more major solvents (amines or alcohols) allows decreasing decomposition temperature to 60-80 °C and working without excessive pressure. We used aqueous solutions of KOH, which dissolve forming KF well, for our work.

The process was carried out in the apparatus equipped with stirrer, dosing the crude material in the form of alcohol alkali (1:1:1) accompanied by 14 hour ageing at 60-80 °C and further rectification. Processes using such method are characterized as "technical" and their warranty storage period is 6 months. Due to the simplicity of apparatus, the method has been implemented commercially, though it is characterized by a large amount of waste. Polyfluorinated compounds practically do not react with gaseous fluorine. Above this point we can observe burning, and sometimes explosions. Low molecular polyfluorinated materials and soot are the main products of this reaction. Fluorinating using catalysts that is iron, cobalt, manganese and nickel fluorides, proved to be more successful. At Fig.2 we can find the results of catalytic fluorination of the "crude material", obtained by electrochemical fluorination of tributylaluminum.

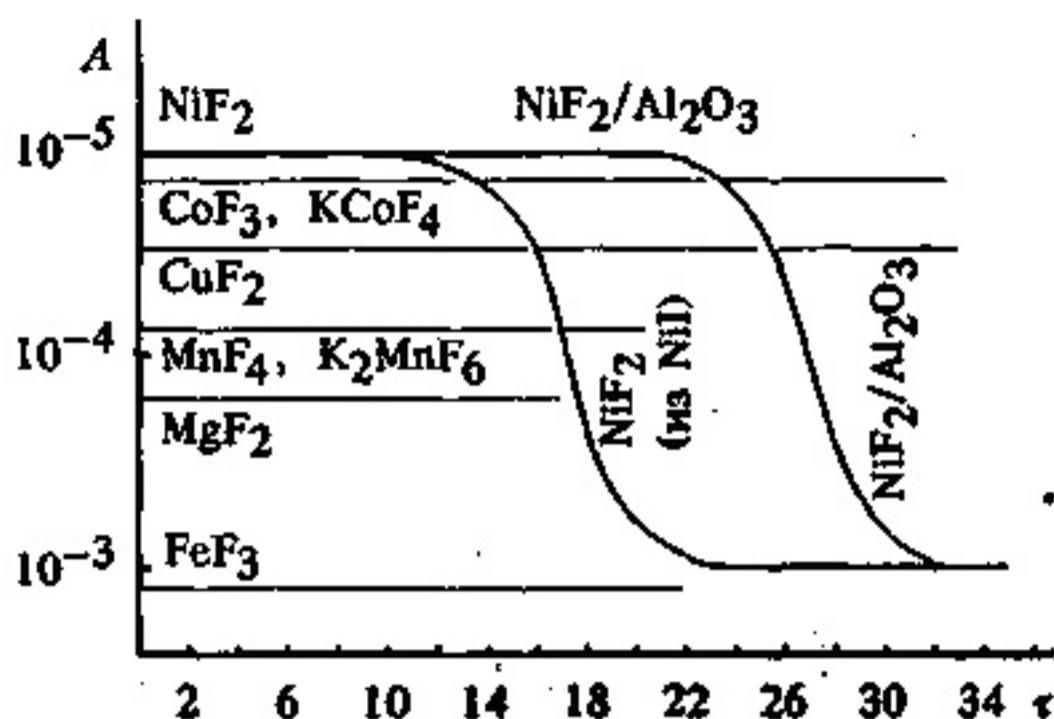


Fig.2. Catalytic Fluorination of Hydrogen Containing Admixtures of the Perfluorotributyl material" (Temperature 420 °C, contact period 13 min., A - amount of ion-fluoride bound (process period (h))

We can see, that fluorination is going in a time gap, at that depending on the nature of fluorination goes with different depth (it was controlled according to the amount of ion-fluoride bound). Hydrogen containing admixtures fluorination goes at a most full grade when using nickel difluoride its activity drops sharply in a few hours time. Cobalt trifluoride properties are close to nickel, catalytic activity lasts much longer and is in between the gap of 200 and 350 hours. In Table 1 the results of fluorination using CoF_3 of some of the "crude material", obtained at electrochemical

Table 10. Parameters of Different "Crude Material" Elemental Fluorine Fluorination Processes

"Crude Material"	T(°C)		Fluorine consumption (mole/mole)	Contact Time (min.)	"Crude Material" content (after) fluorination		
	vaporizer	reactor			Low-boiling products	Target product	Hydrogen containing products
C_5F_{10}	60	230-280	3.3	5	4.5 (6.5)	82.5 (93.5)	13.0 (0)
$(\text{C}_2\text{F}_5)_3\text{N}$	90	270-330	4.0	5	15.5 (19.4)	74.0 (80.6)	10.5 (0)
$(\text{C}_3\text{F}_7)_3\text{N}$	140	320-380	4.9	10	18.4 (24.3)	64.6 (75.7)	17.0 (0)
$(\text{C}_4\text{F}_9)_3\text{N}$	200	350-400	6.0	13	23.5 (32.9)	56.5 (67.1)	20.0 (0)
$(\text{C}_5\text{F}_{11})_3\text{N}$	250	380-420	5.9	16	34.4 (43.4)	48.6 (56.6)	17.0 (0)
$(\text{C}_4\text{F}_9)_2\text{O}$	110	300-350	2.8	6	6.4 (8.2)	83.5 (91.8)	10.1 (0)

According to this method we managed to obtain samples of perfluorinated compounds (fluoride equal to $(1-3) \times 10^{-5}$ mole/l) which are not absorbed in the area of 200 - 320 nm. Such be qualified as "pure", their guaranteed shelf life is 20 years and they can be used in technique of medical preparations and materials. In Table 11 one can find the characteristic of commercial perfluorinated compounds, obtained by additional fluorination of "Crude Material" using elemental fluorine or direct fluorination using cobalt trifluoride as catalyst.

Table 11. Perfluorinated Dielectrics-Heat-Transfers (PFDT) Developed at Federal State Unit RSC "Applied Chemistry"

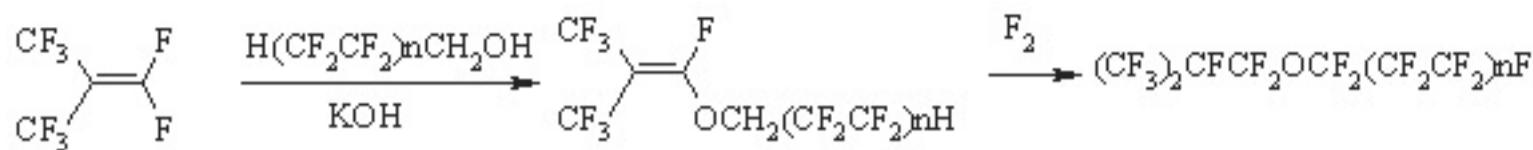
Technical Name	Main Compound	Boiling Point, °C	Melting Point, °C	d_4^{20} , kg/m ³	Specific Volume Resistance Ohm*m (20 °C)	El. Strength KV/cm
PFDT-30	C_5F_{12}	25-35	-125	1660	-	-
PFDT-50	$CF_3(C_2F_5)_2N$	45-50	-163	1670	$1.5 \cdot 10^{13}$	30
PFDT-70	$(C_2F_5)_3N$	65-71	-145	1750	$5.0 \cdot 10^{13}$	30
PFDT-100	$(C_4F_9)_2O$	98-102	-70	1730	$4.0 \cdot 10^{13}$	46
PFDT-130	$(C_3F_7)_3N$	125-132	-65	1840	$3.0 \cdot 10^{14}$	44
PFDT-180	$(C_4F_9)_3N$	178-185	-55	1890	$4.8 \cdot 10^{14}$	40
PFDT-205	$(C_5F_{11})_3N$	195-205	about -50	about 1900	-	40
PFDT-240	$(C_6F_{13})_3N$	235-245	about -50	about 1950	-	-

In our opinion, the major advantage of this approach is the fact, that admixtures do not separate from the main product, and on the contrary, they transform into useful perfluorinated components, which not decrease the quality of target product, but also become suitable for use of composites. Perfluorinated compounds, they also significantly increase the efficiency of fluorine use. The waste, which utilization is a very challenging and complicated task, is very important as well as becoming possible to replace the rectification with distillation, that also simplifies the technology and reduces the cost of it.

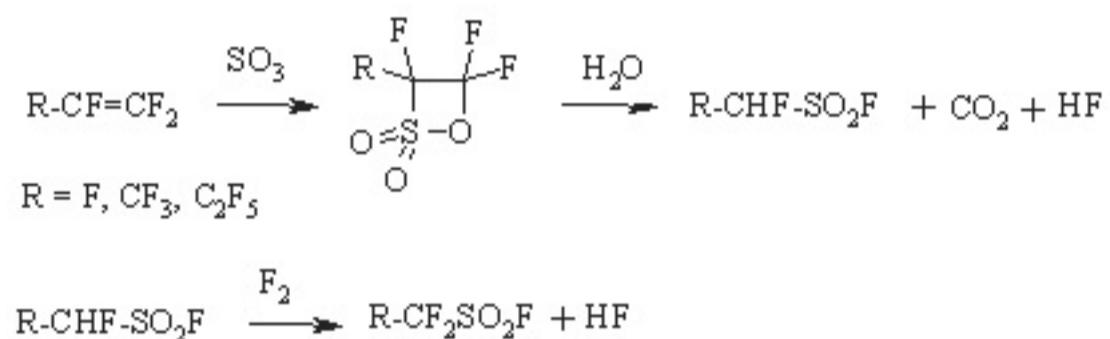
3. Fluorine Containing Semi-Products Synthesis for Creating of New Generation of and Dielectrics

The semi-products of fluororganic synthesis are of interest of production of new materials, such products themselves can find their application, but the base consists of fully fluorinated compounds. Here we shall draw a purification of emissions of plants producing fluororganic compounds products, which a rule contain high toxic agents, for example, perfluoroisobutylene, as an example. At this stage see its transformation into effective liquid dielectric by additional fluorination using elemental fluorine.

Additional fluorination can be carried out using electrochemical fluorination method for compound $(CF_3)_2CHCF_2OC_nF_{2n+1}$ ($n= 1-4$) [60]. This compound is used as solvent for purification systems, chlorine agents, frothers etc.



The second example refers to obtaining of perfluoroalkansulfofluoride, a key semi-product for electrolytes based on lithium bis(perfluoroalkylsulfonylfluoride)imide salt. Here we used obtain cycle opening, decarboxylation and additional elemental fluorine fluorination [61]. Elemental fluorination is carried out at temperature ranging from 0 to 30 °C, the process goes free from forming of destructive fluorination products with the target product yield reaching 97.5 mass.%



Along with polyfluorinated alkansulfofluorides we have studied the fluorination of alkanesulfides. Yield of perfluoroalkanesulfofluorides is 90% for CH_3SO_2F and 82 % for $C_2F_5SO_2F$. Obtaining perfluoroalkanesulfofluorides provides high yield for target product when using standard techniques and available raw materials, that gives us an opportunity to implement it on an industrial scale. Unlike ECF this method provides for period stability of the process and makes the energy costs lower.

4. Production of Ozone-Friendly Chladienes

Hexafluoroethane obtaining methods are mainly based on power-consuming processes ($CF_2=CF_2$). Here we offer hexafluoroethane obtaining method out of tetrafluoroethylene by elemental fluorination in the medium of inert solvent [27,62]. Fluorination is carried out in the perfluorocarbon liquid, containing 8-11 (mass.-%) of stable perfluoromethyl-2-pentafluoroethyl radical at 50-60 °C and fluorine : tetrafluoroethylene ratio = 1:1 - 1.1 mole. This approach is developing the obtaining method of octafluoropropane by fluorination of hexafluoropropene with fluorine influencing hexafluoropropene at temperature ranging from -10 - to +30 °C in the perfluorocarbon liquid (perfluorolefines of composition of $(CF_3)_2CFCR^1=CR^2CF_3$, where $R^1 = F, C_2F_5$; $R^2 = F, CF_3, CF_2CF_2CF_2CF_3$ or linear perfluorinated aliphatic compounds of $CF_3(CF_2)CF$ containing where $n = 5 - 10$), containing 3-8 (mass.-%), stable 1,1,3,3-tetrapentafluoroethylidene difluoropropyl radical [62]. Due to high thermal effect the reaction of direct hexafluoropropene (-658 KJ/mole) was carried out in the liquid perfluorocarbon medium in a designed reactor with combined mixing device. It is stated, that during fluorination of hexafluoropropene stable radical is formed, stable at 20 °C during one-year storage. The developed octafluoropropane (R-218, R-218) obtaining method is characterized by as much as five times higher relative production than actual commercial method for gas-cycle fluorination at CoF_3 [28, 63]. The selectivity by hexafluoropropene amounts to 96-99 %. The method has been implemented at pilot (experimental-industrial) with 200 dm³ reactor. Low-waste, focused at large-tonnage production gas-cycle elemental fluorination technology of hexafluoropropene has been developed. R-218 is applied for engineering and electronics and is an ozone-friendly product.

n-Perfluoropentane [64] is obtained at high yield by elemental fluorine fluorination of n-pentane. Information on fluorination of trichloromethane using metals fluorides in the presence of a catalyst in the solvent medium allowed to come across a trifluoromethane obtaining methane. It was determined, that fluorination of trichloromethane by alkali metals fluorides in the dimethyl ether at 120-150 °C results generally in total substitution of chlorine atoms for fluorine in a. The content of trifluoromethane in gaseous products of fluorination reaches 91.7 % (vol.).

We have conducted a comparative analysis for effectiveness of potassium, sodium, calcium and magnesium fluorides in reactions of haloidhydrocarbons fluorination reactions under conditions of phase-transfer. We have noticed a small effectiveness of potassium fluorides in the reaction with trichloromethane. The suggested synthesis method and a reactor are successfully approved at an experimental-industrial scale. It was determined, that fluorination of trifluoromethane using fluorine, containing oxygen (0.05%) over tetrafluoromethane at 100-400 °C in reactor filled with metallic nozzle made of copper-chrome results in formation of terafluoromethane (products' composition 99.8 % CF_4 , 0.2 % C_2F_6).

It allowed increasing the conversion of raw materials and selectivity of the process and lowering of inputs. Tetrafluoromethane obtaining method by fluorinating of different grades of coal containing carbon (from 5 to 25% mass.) at temperature ranging from 700 to 1200 °C was developed. It should be mentioned, that fluorination is conducted either using pure fluorine or anode gas, formed during KF-2HF mixture and containing up to 10 (mass.) % of anhydrous hydrogen fluoride. It allows to skip labour-intensive and power-consuming stage of fluorine purification.

At the same time the presence of anhydrous hydrogen fluoride allows to depart from solvent mixture. The availability of anhydrous hydrogen fluoride results in decreasing of excessive heat of fluorinating reaction, improves heat exchange, increases the process selectivity due to lowering of concurrent high-molecular perfluoroalkanes.

The use of activated carbon additives decreases the process explosive risk, leads to combustion faster reaching of the stable stage and, therefore to increasing of CF_4 yield. The concentration higher than 25(mass.)% makes the method economically irrational.

Conclusion

As can be seen from the data, listed in this review, the conception of synthesis of perfluorocompounds by fluorination using elemental fluorine both in a pure form and in the presence of a catalyst found its experimental approval. We also should mark the importance of results of such approach not only and not as much as for obtaining methods of practically necessary perspective compounds but for economical practicability. Thus, it is manageable to increase the yield of perfluorinated compounds sharply, to improve their quality, to increase significantly the efficiency of fluorine use and to simplify the process itself and obtaining technology of many substances. The results showed the urgency and timeliness of setting such a problem and a need for its boosted solving. Laid as a foundation of conception mentioned above, proved to be productive and its implementation for commercial production will stimulate a change in the production men's view regarding the question of using elemental fluorine for production.

References

1. Chemistry of Organic Fluorine Compound. II. Eds. M. Hydlicky, A.E. Pavlath/ Washington Chem. Soc., 1995, 1296 c. (ACS Monography, N 187).
2. Енэтани М., Есгмура Т., В кн. Новое в технологии соединений фтора. Под ред. Н. И. Японск. Под ред. А.В.Фокина. М. :Мир, 1984, с. 289-446

3. Organofluorine Chemistry. Principles and Commercial Application. Eds. Banks R.E., Sm J.C., Plenum Publishing Corporation, 1994.

4. Рахимов А.И. Химия и технология фторорганических соединений. -М. : Химия, -1986.

5. Moldavsky D.D., Furin G.G. J. Fluorine Chem., 1998, v. 87, p. 111-121. 6. Moldavsky D.D., Kaurova G.I., Furin G.G. J. Fluorine Chem., 1999, v. 94, p. 157-167.

7. Новые фторорующие реагенты в органическом синтезе. Под ред. Л.С.Герман, Новосибирск : Наука, 1987, 256 с.

8. Furin G.G., G.P. Gambaretto Direct Fluorination of Organic Compounds. CLEUP Coop Editrice Universita di Padova, Italy, 1996, 212p. 9. Shimizu M., Hiyama T. Angew. Chem. Int. Ed. v. 44, N 2, p. 214-231.

10. Tavener S.J., Clark J.H. J. Fluorine Chem., 2003, v. 123, N 1, p. 31-36.

11. Drakesmith F.G. Top. Curr. Chem., 1997, v. 193, p. 197-242.

12. Shimizu M., Hiyama T. Angew. Chem. Int. Ed. Engl., 2004, v. 44 N 2, p. 214-231.

13. Suzuki Y., Watanabe K., Yanase K. (Asahi Glass Co., Ltd., Japan), PCT Int. Appl. WO (2004); Chem. Abstr., 2004, v. 140, 356951.

14. Tavener S.J., Clark J.H. J. Fluorine Chem., 2003, v. 123, N 1, p. 31-36.

15. Kirsch P., Hahn A. (Merck Pat. G.m.b.H., Germany) Ger. Offen DE 10258577 (2003); 2004, v. 139, 133074.

16. Moldavski D.D., Kaurova G.T., Bispen T.A., Furin G.G. J. Fluorine Chem., 1993, v. 63, p. 19-24.

17. Шеннард У., Шартс К. Органическая химия фтора, М.: Мир, 1972, 480 с.

18. Lagow R.J., Margrave J.L. Direct Fluorination : A "New" Approach to Fluorine Chemistry. inorganic Chemistry/Ed. S.J.Lippard, -Interscience Publication, -John Wiley and Sons : New York, P.161-210.

19. Захаров В.Ю., Денисенков А.К., Новиков М.Д. // Ж.орган. химии, 1994, т. 30, вып 1847.

20. Биспен Т.А., Михайлова Т.В., Молдавский Д. Д. и др. // Ж. прикл. химии, 1996, т. 112-119.

21. Advances in Fluorine Chemistry Eds. M.Stacy. J.C.Ta-tlow, A.G.Sharpe. London: Butterworth-Heinemann, 1990-1991, v. 111, 570 p.

22. Bockemuller W. // Lieb. Ann., 1933, bd. 506, s. 20- 23.

23. Wilkinson J.A. // Chem. Rev., 1992, v. 92, p. 505-519.

24. Биспен Т.А., Молдавский Д.Д., Фурин Г.Г. // Ж.прикл. химии, 1998, т. 71, вып. 8, Chem. Abstr. 1999, v. 130, 211033.

25. Биспен Т.А., Молдавский Д.Д., Фурин Г.Г. // Ж. прикл. химии, 1998, т. 71, № 6 Chem. Abstr., 1999, v. 130, 224586.

26. Kobayashi M., Ishii F., Tomioka H., Oka K. 12th European Symposium on Fluorine Chemistry, Sep. 2, 1998, Berlin, Germany. Anstracts, A36.

27. Терещенко Г.Ф., Кузнецов А.С., Ильин А.Н., и др. // Пат. 2124493 Россия. Опубл. 1 (1999); С. 332. РЖХим. 1999. 11Н167П. Chem. Abstr., 2000, v. 133, 176946s.

28. Абрамов О.Б., Александрова Т.С., Арасланов Г.Г. и др. Пат. 2185363Россия (20017-04; Chem. Abstr., 2004, v. 139, 54551.

29. Watanabe K., Okazoe T., Tatematsu S. (Asahi Glass Co., Ltd., Japan) Eur. Pat. Appl. EP 96 Chem. Abstr., 2000, v. 132, 51455.

30. Okada N., Kato M., Yoshinaga M. (Tokuyama Soda Co., Ltd., Japan) Jpn. Kokai Tokkyo Koho (1997), Cl, B 01 D 053-70; Chem. Abstr., 1998, v. 127, 98975.

31. Rodgers A.S. J. Phys. Chem., 1965, v. 69, N 1, p. 254-257.

32. Scherer K.V., Ono T., Jamanouchi J. Am. Chem. Soc., 1985, v. 107, N 3, p. 718-719.

33. Ono H., Nakajo T., Arai T., Oi T. (Showa Denko K.K., Japan), Jpn. Kokai Tokkyo Koho JP 0925 Cl, C 07 C 019-08; Chem. Abstr., 1998, v. 127, 331191.

34. Пашкевич Д.С., Мухортов Д.А., Алексеев Ю.Т., Асович В.С. Ж. прикл. химии, 2002, 1269-1274.

35. Seki E., Aoyama H. (Daikin Industries, Ltd., Japan) Jpn. Kokai Tokkyo Koho JP 11124352 (1996) C 041-22; Chem. Abstr., 1999, v. 130, 337838.

36. Ono T., Yamanouchi K., Scherer K.V. J. Fluorine Chem., 1995, v. 73, p. 267-272.

37. Молдавский Д.Д., Биспен Т.А., Фурин Г.Г., Жужгов Э.Л. // Ж. прикл. химии, 1996, 636-644; Chem. Abstr., 1996, v. 69, p. 636-644.

38. Weinmaye V. // J. Org. Chem., 1963, v. 28, N 2, p. 492- 493.

39. Фурин Г.Г., Дубовенко З.Д., Молдавский Д.Д. // Ж. прикл.химии, 1996, т. 69, № 1, с. 636-644.

40. Справочник химика. т. 1 / Под ред. Б.П.Никольского. Л.: Химия, 1971, с. 925-930.

41. Молдавский Д.Д., Шкультецкая Л.В., Фурин Г.Г. З-я Международная конференция «Фторсодержащие технологии и применение фторсоединений» СТАФ`2001.6-9 июня 2001, С. Петербург. Тез.Докл.Р1-21,с. 156-157.

42. Oharu K., Takagi Y., Murotani E. (Asahi Glass Co., Ltd., Japan), Jpn. Kokai Tokkyo Koho JP 2004-056694 (Cl. C 07 C 51/60) (2004); Chem. Abstr., 2004, v. 140, 406548q.

43. Okazoe T., Watanabe K., Tatematsu S., Murofushi H. (Asahi Glass Co., Ltd., Japan), PCT 2000 056694 (Cl. C 07 C 059-135), Chem. Abstr., 2000, v. 133, 266514.

44. Okazoe T., Watanabe K., Itoh M., Shirakawa D., Tatematsu S., Takagi H. (Asahi Glass Co., Ltd., Japan) PCT Int. Appl. WO 2002 018314 (Cl. C 07 C 049-167, C 07 C 051-58, C 07 C 059-135); Chem. Abstr., 2003, v. 136, 216751.

45. Fontana G., Navarrini W. (SolvaySolexisS.p.A.), Заявка 1440993 ЕПВ (2004), МПК7 С 05.08-19Н.82П.

46. Suzuki Y., Watanabe K., Yanase K., (Asahi Glass Co., Ltd., Japan) PCT Int. Appl. WO 2004-056694 (Cl. C 07 C 067-287; Chem. Abstr., 2004, v. 140, 356951.

47. Okazoe T., Murotani E., Watanabe K., Itoh M., Shirakawa D., Kawahara K., Kaneko I., Tatematsu S. (Asahi Glass Co., Ltd., Japan) PCT Int. Appl. WO 2004-056694 (Cl. C 07 C 067-287; Chem. Abstr., 2004, v. 140, 356951.

Fluorine Chem., 2004, v. 125, p. 1695-1701.

48. Okamoto H., Okazoe T., Watanabe K., Takagi H. (Asahi Glass Co., Ltd., Japan) PCT Int. A 026679 (2002); Chem. Abstr., 2003, v. 136, 294533.

49. Okazoe T., Watanabe K., Itoh M., Shirakawa D., Kawahara K., Tatematsu S. J. Fluorine Cl 126, p. 521-527.

50. Молдавский Д.Д., Фурин Г.Г. // Ж. общ. химии, 1996, т. 66, вып. 12, с. 1995-2002; v. 126, 225259.

51. Корнилов В.В., Костевв Р.А., Максимов Б.Н., и др. // Ж. прикл.химии, 1995, т. 68, 1418.

52. Степей М., Тэтпуу Д.К. Успехи химии фтора. т. 1. М.: Химия, 19646 576 с.

53 Захаров В.Ю., Денисов А.К., Новикова М.Д. // Ж. орг. химии, 1994, т. 30, № 12, с. 1

54. Захаров В.Ю., Денисов А.К., Новикова М.Д. Тез. докл. Междунар. конф. «Химия, применение фторсодержащих соединений в промышленности». СПб, Россия, 1994, с. 11

55. Молдавский Д.Д., Фурин Г.Г., Шкультецкая Л.В., Эйфман Б.Я. // Ж. прикл. химии вып. 6, с. 976-978; Chem. Abstr., 2004, v. 138, 204583.

56. Розовский А.Я. Катализатор и реакционная среда. М.: Наука, 1988. 303 с.

57. Асович В.С.. Костеев Р.А. // Ж. прикл.химии, 1994, т. 67, № 8, с. 1320-1323.

58. Сухотин А.М., Зотиков В.С. Химическое сопротивление материалов, Л.: Химия, 197

59. Биспен Т.А., Михайлова Т.В., Молдавский Д.Д., и др. // Ж. прикл. химии, 1996, т. 112-119.

60. Hansen J.C. Pat. U.S. 5474657 (1995); РЖХим.1997, 23Н132П.

61. Барабанов В.Г., Боруцкая Г.В., Биспен Т.А., и др. Пат. России 2237659 (2003); 309/80, 303/22, БИ № 28 (2004); РЖХим., 05.02 – 19Н. 121 П.

62. Денисенков В.Ф., Ильин А.Н., Волков В.Н., и др. // Заявка 93036358.04 Россия. Бюл. 22. (1996); РЖХим. 1997. 14Н 108 П; Пат. 2074162 Россия. Опубл. 1997; Бюл. (1998); РЖХим. 1998. 15Н118П; Chem. Abstr., 1997, v. 127, 176171m.

63. Ильин А.Н., Иванова Л.М. // Международная научно-техническая конференция «химической технологии и материалов. Пермь [1997] : Тез. Докл. – Пермь, 1997, с. 203; 12Н 130.

64. Watanabe K., Okazoe T., Tatematsu S. (Asahi Glass Co., Ltd., Japan) , Eur. Pat.Appl. EP 96 Chem. Abstr., 2000, v. 132, 51455.

65. Ильин А.Н., Иванова Л.М. VI Всесоюзная конференция по химии фторорганических 26-28 июня 1990. Новосибирск. Тезисы докладов, с. 194.

66. Уклонский И.П., Денисенков В.Ф., Ильин А.Н., и др. // Пат. 2181352 Россия. Опубл. 11. (2002).

67. Уклонский И.П., Денисенков В.Ф., Ильин А.Н., и др. // Пат. 2181351 Россия. Опубл. 11. (2002).

