

## ADDITIONAL FLUORINATION OF PARTLY FLUORINATED ORGANIC COMPOUNDS BY ELEMENTAL FLUORINE, AN OBTAINING METHOD FOR PRACTICAL PURPOSES OF FLUORINE MATERIALS

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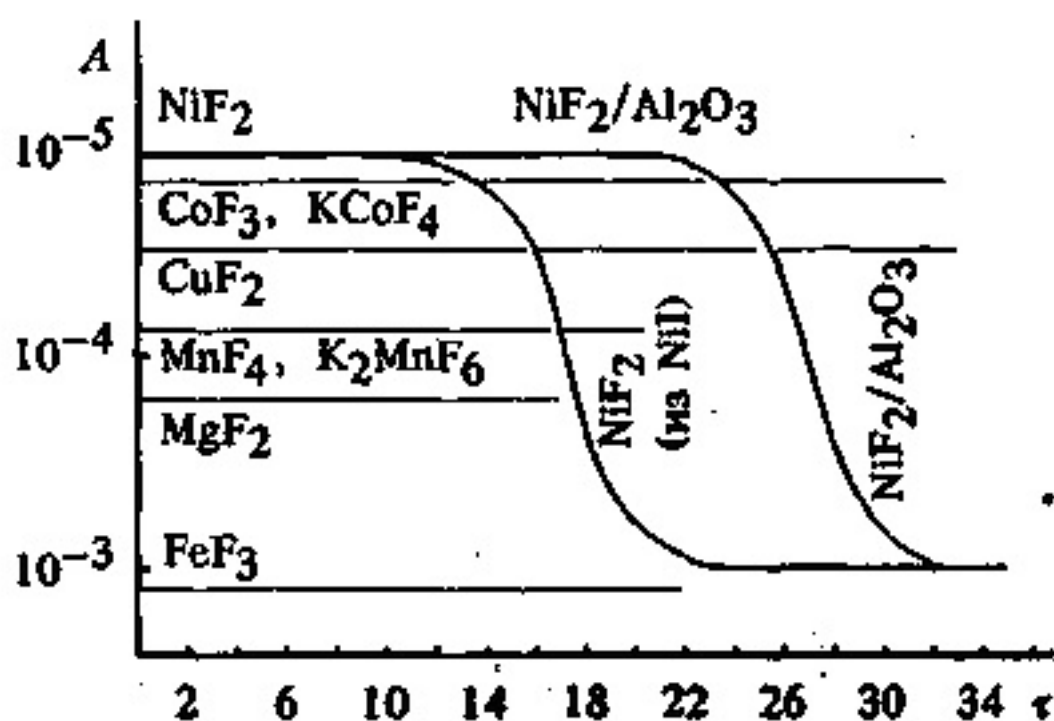
*(continuation)*

### 2. Perfluorinated Organic Compounds Purification

Data listed above allowed us to draw an assumption, that such an approach can be successful for deep purification of perfluorinated compounds ("crude materials") obtained using ECF method. All known methods are based on destruction of hydrogen containing admixtures. We take into account that their content in the reaction mixtures reaches 30%, then these materials are recognized as wholly satisfactory. Another approach for purification of PFOC (perfluorinated organic compounds) is in additional fluorination of hydrogen containing admixtures. This approach implementation allows increasing of yield of PFOC, lowering of waste products, simplifying technology and as a result decreasing the cost of target products.

The known method of purification is in high concentration aqua alkali (85-90%) treatment at 60-80 °C. This method has a number of essential disadvantages, which hampers its application in production. Among them are: a need of working under pressure of 13-15 bar, high melting point of high concentration alkali and a related to that danger of blocking armature and communications, and also a need of special alloys for reactor making, as common stainless steel are up to corrosive cracking [58, 59], that water displacement by more major solvents (amines or alcohols) allows decreasing decomposition temperature to 60-80 °C and working without excessive pressure. We used aqueous solutions of KOH, which dissolve forming KF well, for our work.

The process was carried out in the apparatus equipped with stirrer, dosing the crude material into alcohol alkali (1:1:1) accompanied by 14 hour ageing at 60-80°C and further rectification. Products obtained using such method are characterized as "technical" and their warranty storage period is 6 months. Due to simplicity of apparatus, the method has been implemented commercially, though it is characterized by a large amount of waste. Polyfluorinated compounds practically do not react with gaseous fluorine. Above this point we can observe burning, and sometimes explosions. Low molecular polyfluorinated compounds and soot are the main products of this reaction. Fluorinating using catalysts that is iron, cobalt, manganese and nickel fluorides, proved to be more successful. At Fig.2 we can find the results of catalytic fluorination of the "crude material", obtained by electrochemical fluorination of tributylamine.



**Fig.2.** Catalytic Fluorination of Hydrogen Containing Admixtures of the Perfluorotributyl "material" (Temperature 420 °C, contact period 13 min., A - amount of ion-fluoride bound ( process period (h) )

We can see, that fluorination is going in a time gap, at that depending on the nature of fluorination goes with different depth (it was controlled according to the amount of ion-fluoride bound). Hydrogen containing admixtures fluorination goes at a most full grade when using nickel difluoride, its activity drops sharply in a few hours time. Cobalt trifluoride properties are close to nickel trifluoride, its catalytic activity lasts much longer and is in between the lap of 200 and 350 hours. In Table 1 the results of fluorination using CoF<sub>3</sub> of some of the "crude material", obtained at electrochemical

**Table 10.** Parameters of Different "Crude Material" Elemental Fluorine Fluorination Processes

"Crude Material"	T(°C)		Fluorine consumption (mole/mole)	Contact Time ( min.)	"Crude Material" content (after) fluorination		
	vaporizer	reactor			Low-boiling products	Target product	Hydrogen containing products
C <sub>5</sub> F <sub>10</sub>	60	230-280	3.3	5	4.5 (6.5)	82.5 (93.5)	13.0 (0)
(C <sub>2</sub> F <sub>5</sub> ) <sub>3</sub> N	90	270-330	4.0	5	15.5 (19.4)	74.0 (80.6)	10.5 (0)
(C <sub>3</sub> F <sub>7</sub> ) <sub>3</sub> N	140	320-380	4.9	10	18.4 (24.3)	64.6 (75.7)	17.0 (0)
(C <sub>4</sub> F <sub>9</sub> ) <sub>3</sub> n	200	350-400	6.0	13	23.5 (32.9)	56.5 (67.1)	20.0 (0)
(C <sub>5</sub> F <sub>11</sub> ) <sub>3</sub> N	250	380-420	5.9	16	34.4 (43.4)	48.6 (56.6)	17.0 (0)
(C <sub>4</sub> F <sub>9</sub> ) <sub>2</sub> O	110	300-350	2.8	6	6.4 (8.2)	83.5 (91.8)	10.1 (0)

According to this method we managed to obtain samples of perfluorinated compounds (fluoride equal to  $(1-3) \cdot 10^{-5}$  mole/l) which are not absorbed in the area of 200 - 320 nm. Such can be qualified as "pure", their guaranteed shelf life is 20 years and they can be used in technique of medical preparations and materials. In Table 11 one can find the characteristic of commercial perfluorinated compounds, obtained by additional fluorination of "Crude Material" using either direct fluorination using cobalt trifluoride as catalyst.

**Table 11.** *Perfluorinated Dielectrics-Heat-Transfers (PFDT) Developed at Federal State Unit RSC "Applied Chemistry"*

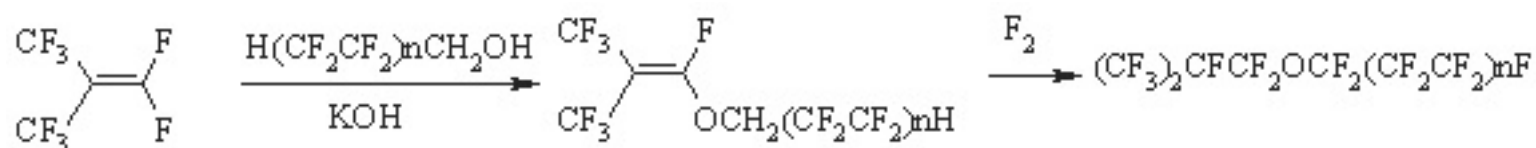
<i>Technical Name</i>	<i>Main Compound</i>	<i>Boiling Point, °C</i>	<i>Melting Point, °C</i>	<i>d<sub>4</sub><sup>20</sup>, kg/m<sup>3</sup></i>	<i>Specific Volume Resistance Ohm*m (20 °C)</i>	<i>Electrical Strength KV/mm</i>
PFDT-30	C <sub>5</sub> F <sub>12</sub>	25-35	-125	1660	-	-
PFDT-50	CF <sub>3</sub> (C <sub>2</sub> F <sub>5</sub> ) <sub>2</sub> N	45-50	-163	1670	1.5 · 10 <sup>13</sup>	30
PFDT-70	(C <sub>2</sub> F <sub>5</sub> ) <sub>3</sub> N	65-71	-145	1750	5.0 · 10 <sup>13</sup>	30
PFDT-100	(C <sub>4</sub> F <sub>9</sub> ) <sub>2</sub> O	98-102	-70	1730	4.0 · 10 <sup>13</sup>	46
PFDT-130	(C <sub>3</sub> F <sub>7</sub> ) <sub>3</sub> N	125-132	-65	1840	3.0 · 10 <sup>14</sup>	44
PFDT-180	(C <sub>4</sub> F <sub>9</sub> ) <sub>3</sub> N	178-185	-55	1890	4.8 · 10 <sup>14</sup>	40
PFDT-205	(C <sub>5</sub> F <sub>11</sub> ) <sub>3</sub> N	195-205	about -50	about 1900	-	40
PFDT-240	(C <sub>6</sub> F <sub>13</sub> ) <sub>3</sub> N	235-245	about -50	about 1950	-	-

In our opinion, the major advantage of this approach is the fact, that admixtures do not separate from main product, and on the contrary, they transform into useful perfluorinated components, which do not decrease the quality of target product, but also become suitable for use of composition of perfluorinated compounds, they also significantly increase the efficiency of fluorine use. The problem of waste, which utilization is a very challenging and complicated task, is very important as well as becoming possible to replace the rectification with distillation, that also simplifies the technology and the cost of it.

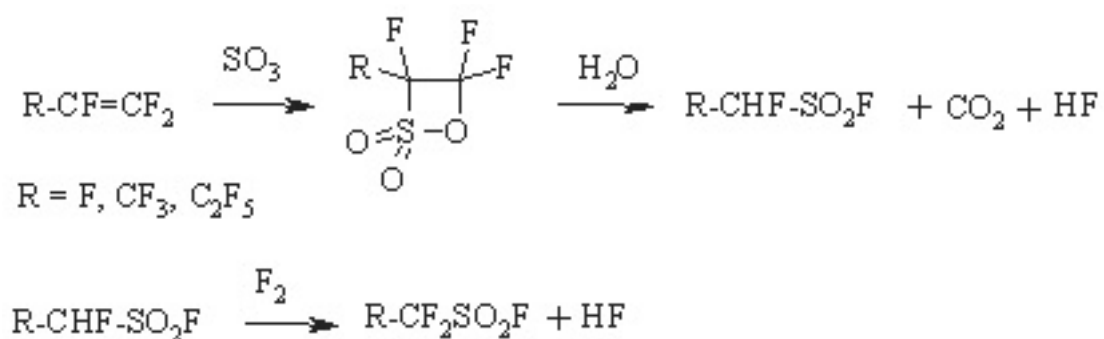
### 3. Fluorine Containing Semi-Products Synthesis from Creating of New Generation of Fluorine Compounds and Dielectrics

The semi-products of fluororganic synthesis are of interest for production of new materials. Such products themselves can find their application, but the base consists of fully fluorinated compounds. Here we shall draw a purification of emissions of plants producing fluororganic compounds produced by a rule contain high toxic agents, for example, perfluoroisobutylene, as an example. At this distillation we see its transformation into effective liquid dielectric by additional fluorination using elemental fluorine.

Additional fluorination can be carried out using electrochemical fluorination method for compounds  $(CF_3)_2CHCF_2OC_nF_{2n+1}$  ( $n = 1-4$ ) [60]. This compound is used as solvent for purification systems, chlorine agents, frothers etc.



The second example refers to obtaining of perfluoroalkanesulfofluoride, a key semi-product for electrolytes based on lithium bis(perfluoroalkylsulfonylfluoride)imide salt. Here we used electrochemical cycle opening, decarboxylation and additional elemental fluorine fluorination [61]. Electrochemical fluorination is carried out at temperature ranging from 0 to 30 °C, the process goes free from forming of destructive fluorination products with the target product yield reaching 97.5 mass. %



Along with polyfluorinated alkane sulfofluorides we have studied the fluorination of alkanesulfonylfluorides. The yield of perfluoroalkanesulfofluorides is 90% for  $CH_3SO_2F$  and 82 % for  $C_2F_5SO_2F$ . Obtaining of perfluoroalkanesulfofluorides provides high yield for target product when using standard techniques and available raw materials, that gives us an opportunity to implement it on an industrial scale. Unlike ECF this method provides for period stability of the process and makes the energy cost lower.

#### 4. Production of Ozone-Friendly Chladones

Hexafluoroethane obtaining methods are mainly based on power-consuming processes (pyrolysis of  $CF_2=CF_2$ ). Here we offer hexafluoroethane obtaining method out of tetrafluoroethylene by electrochemical fluorination in the medium of inert solvent [27,62]. Fluorination is carried out in the medium of perfluorocarbon liquid, containing 8-11 (mass.%) of stable perfluoromethyl-2-pentafluoroethyl radical at 50-60 °C and fluorine : tetrafluoroethylene ratio = 1:1 - 1.1 mole. This approach allows developing the obtaining method of octafluoropropane by fluorination of hexafluoropropene with elemental fluorine influencing hexafluoropropene at temperature ranging from -10 - to +30 °C in the medium of perfluorocarbon liquid (perfluoroolefines of composition of  $(CF_3)_2CFCR^1=CR^2CF_3$ , where  $R^1 = F, C_2F_5$ ,  $R^2 = F, CF_3, CF_2CF_2CF_2CF_3$  or linear perfluorinated aliphatic compounds of  $CF_3(CF_2)_nCF_3$  where  $n = 5 - 10$ ), containing 3-8 (mass.%) stable 1,1,3,3-tetrafluoro-2-pentafluoroethyldifluoropropyl radical [62]. Due to high thermal effect the reaction of direct fluorination of hexafluoropropene (-658 kJ/mole) was carried out in the liquid perfluorocarbon medium in a specially designed reactor with combined mixing device. It is stated, that during fluorination of hexafluoropropene a stable radical is formed, stable at 20 °C during one-year storage. The developed octafluoropropane (R-218, R-218) obtaining method is characterized by as much as five times higher relative productivity compared to actual commercial method for gas-cycle fluorination at  $CoF_3$  [28, 63]. The selectivity by hexafluoroethane amounts to 96-99 %. The method has been implemented at pilot (experimental-industrial) scale with 200 dm<sup>3</sup> reactor. Low-waste, focused at large-tonnage production gas-cycle electrochemical fluorination technology of hexafluoropropene has been developed. R-218 is applied for engineering and electronics and is an ozone-friendly product.

n-Perfluoropentane [64] is obtained at high yield by elemental fluorine fluorination of n-pentane. Information on fluorination of trichloromethane using metal fluorides in the presence of a catalyst in the solvent medium allowed to come across a trifluoromethane obtaining method. It was determined, that fluorination of trichloromethane by alkali metal fluorides in the dimethyl ether at 120-150 °C results generally in total substitution of chlorine atoms for fluorine in a content of trifluoromethane in gaseous products of fluorination reaches 91.7 % (vol.).

We have conducted a comparative analysis for effectiveness of potassium, sodium, calcium fluorides in reactions of halohydrocarbons fluorination reactions under conditions of phase-transfer catalysis. We have noticed a small effectiveness of potassium fluorides in the reaction with trichloromethane. The suggested synthesis method and a reactor are successfully approved at an experimental-industrial scale. It was determined, that fluorination of trichloromethane using fluorine, containing oxygen (0.05 %), results in over tetrafluoromethane at 100-400 °C in reactor filled with metallic nozzle made of copper-chrome results in formation of tetrafluoromethane (products' composition 99.8 % CF<sub>4</sub>, 0.2 % C<sub>2</sub>F<sub>6</sub>).

It allowed increasing the conversion of raw materials and selectivity of the process and lowering inputs. Tetrafluoromethane obtaining method by fluorinating of different grades of coal containing carbon (from 5 to 25% mass.) at temperature ranging from 700 to 1200 °C was developed. It was mentioned, that fluorination is conducted either using pure fluorine or anode gas, formed during KF-2HF mixture and containing up to 10 (mass.) % of anhydrous hydrogen fluoride. It allows avoiding a labour-intensive and power-consuming stage of fluorine purification.

At the same time the presence of anhydrous hydrogen fluoride allows to depart from solvent mixture. The availability of anhydrous hydrogen fluoride results in decreasing of excessive heat of fluorinating reaction, improves heat exchange, increases the process selectivity due to lowering of concurrent high-molecular perfluoroalkanes.

The use of activated carbon additives decreases the process explosive risk, leads to faster reaching of the stable stage and, therefore to increasing of CF<sub>4</sub> yield. The concentration higher than 25(mass.)% makes the method economically irrational.

## Conclusion

As can be seen from the data, listed in this review, the conception of synthesis of perfluorinated compounds by fluorination using elemental fluorine both in a pure form and in the presence of catalysts has found its experimental approval. We also should mark the importance of results of such approach not only and not as much as for obtaining methods of practically necessary perspective compounds but for economical practicability. Thus, it is manageable to increase the yield of perfluorinated compounds sharply, to improve their quality, to increase significantly the efficiency of fluorine use and to simplify the process itself and obtaining technology of many substances. This study showed the urgency and timeliness of setting such a problem and a need for its boosted solution. The laid as a foundation of conception mentioned above, proved to be productive and its implementation for commercial production will stimulate a change in the production men's views regarding the question of using elemental fluorine for production.

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